著者 | Ako Olga. Y., Kitamura Y., Intabon K., Satake T.
---|---
タイトル | Bioresource technology
巻 | 99
号 | 14
ページ | 6305-6310
年 | 2007-09
doi | 10.1016/j.biortech.2007.12.016

(C) 2007 Elsevier Ltd.
URL | http://hdl.handle.net/2241/100091
Steady State Characteristics of Acclimated Hydrogenotrophic Methanogens on Inorganic Substrate in Continuous Chemostat Reactors

Olga. Y. Ako¹; Y. Kitamura²*, K. Intabon²; T. Satake²

¹Doctoral Program in Bioindustrial Sciences, University of Tsukuba, Japan

²Graduate School of Life and Environmental Sciences, University of Tsukuba, 1-1-1 Tennodai Tsukuba Ibaraki 305-8572, Japan

*Corresponding author: Graduate School of Life and Environmental Sciences, University of Tsukuba, 1-1-1 Tennodai, Tsukuba, Ibaraki 305-8572, Japan; tel & fax +81 029-853-4655;
e-mail, kitamura@sakura.cc.tsukuba.ac.jp
Abstract

A Monod model has been used to describe the steady state characteristics of the acclimated mesophilic hydrogenotrophic methanogens in experimental chemostat reactors. The bacteria were fed with mineral salts and specific trace metals and a H₂/CO₂ supply was used as a single limited substrate. Under steady state conditions, the growth yield ($Y_{CH₄}$) reached 11.66 g cells per mmol of H₂/CO₂ consumed. The daily cells generation average was $5.67 \times 10^{11}$, $5.25 \times 10^{11}$, $4.2 \times 10^{11}$ and $2.1 \times 10^{11}$ cells/L-culture for the dilutions 0.071/d, 0.083/d, 0.1/d and 0.125/d, respectively. The maximum specific growth rate ($\mu_{max}$) and the Monod half-saturation coefficient ($K_s$) were $0.15/d$ and $0.82 \text{ g/L}$, respectively. Using these results, the reactor performance was simulated. During the steady state, the simulation predicts the dependence of the H₂/CO₂ concentration ($S$) and the cell concentration ($X$) on the dilution rate. The model fitted the experimental data well and was able to yield a maximum methanogenic activity of $0.24 \text{ L CH}_₄/g \text{ VSS.d}$. The dilution rate was estimated to be $0.1/d$. At the dilution rate of $0.14/d$, the exponential cells washout was achieved.

Keywords: Hydrogenotrophic methanogens; chemostat; steady state; H₂/CO₂ gas; simulation; trace metals
1. Introduction

Extensive research has demonstrated the capability of methanogenic bacteria to grow on molecular hydrogen (H$_2$) and utilize carbon dioxide (CO$_2$) as an energy source (Daniels et al., 1984; Jones et al., 1985). The methanogens are inhabitants of the anaerobic fermentor, which is currently regarded as an attractive process for the degradation of various types of organic matter into methane and other by-products.

The construction of a mathematical model is obviously a crucial step in the design, control and operation of a fermentor (Bastone, 2006). Based on engineering literature, several models have been proposed to simulate and improve the fermentor performance through the supply of organic substrates (Siegrist et al., 2002; Nopharatana et al., 2003). The Monod kinetics model, which is the simplest approach, relates the specific growth rate of the biomass ($\mu$) (1/d) to the residual substrate concentration ($S$) (g/L).

$$\mu = \frac{\mu_{\text{max}} S}{K_S + S} \quad (1)$$

where $\mu_{\text{max}}$ is the maximum specific biomass growth rate and $K_S$ is the half-saturation coefficient (g/L). This relationship has been used to model the single substrate H$_2$ consumption in the presence of another substrate (Robinson
and Tiedje, 1982). It has also been used to model anaerobic acidogenesis (Demirel and Yenigün, 2002). However, there is no report regarding the use of the Monod kinetics model for acclimated hydrogenotrophic methanogens under steady state continuous cultivation with recirculation of the single substrate H$_2$/CO$_2$. The chemostat proposed by Tang et al., 1997 was associated with steady state cultivation that provided a better conversion ratio of H$_2$/CO$_2$ to methane and carbon dioxide (Valentine et al., 2004). Four chemostat reactors were used with varying rates of flow of the inorganic medium. The objectives were, firstly, to attain a steady state chemostat cultivation of H$_2$/CO$_2$-dependant methanogens and measure the limiting supply of substrate, then to apply the Monod relationship to standardize the characteristics of H$_2$/CO$_2$ gas fermentation. The parameters obtained would provide data for the creation of a generic model for the dynamic simulation of biogas production from a methanogen culture using mixed H$_2$/CO$_2$ gas as the substrate.

2. Materials and Methods

2.1. Acclimation of hydrogenotrophic methanogens

Anaerobic activated sludge (2.5 L) obtained from a domestic waste water
treatment plant (Ibaraki, Japan) was acclimated in duplicate 5 L reactors at mesophilic temperatures for 7 months; H₂/CO₂ (80:20, v/v) gas was used as source of energy and carbon. Using a 2 L gas bag, the gas substrate was recirculated at 0.08 MPa. The archaea cultivation procedure (Sowers and Noll, 1995) was implemented and continued until H₂/CO₂-dependant methanogens predominated the culture. The physical and chemical compositions of the acclimated sludge obtained were averaged from the 2 reactors and are shown in Table 1. According to these results, the acetic acid concentration was nil and 56.6% methane was produced. The absence of acetic acid indicates the possibility that methane production from substrates other than the H₂/CO₂ gas mixture can be excluded.

2.2. Epifluorescent microscopy analysis

The acclimated sludge samples were filtered using a polycarbonate black filter with 0.22 μm pore diameter. Using ethidine bromide (Sigma-Aldrich, Poland) as the stain, the sludge samples were observed under an ultra-microscope (OLYMPUS, BX 50, Japan). The apparently uniform blue autofluorescence verified the purity of the culture. A morphological examination of the bacteria revealed long rod-shaped cells and cocci.
A modified version of the medium used by Yang et al. (2004) was applied; the final composition was as follows: mineral nutrients (in g/L of demineralized water) including K$_2$HPO$_4$, 3.4; KH$_2$PO$_4$, 3.4; Na$_2$CO$_3$, 2.54; NH$_4$Cl, 2.13; and trace metals (in mg/L of demineralized water) including MgSO$_4$ \cdot 7$\text{H}_2$O, 600; MnSO$_4$ \cdot 5$\text{H}_2$O, 5.3; NiCl$_2$ \cdot 6$\text{H}_2$O, 125; FeSO$_4$ \cdot 7$\text{H}_2$O, 28; CoCl$_2$ \cdot 6$\text{H}_2$O, 10; ZnSO$_4$ \cdot 7$\text{H}_2$O, 30; CuSO$_4$ \cdot 5$\text{H}_2$O, 8; AlK(SO$_4$)$_2$ \cdot 12$\text{H}_2$O, 1; CaCl$_2$ \cdot 2$\text{H}_2$O, 40; H$_3$BO$_4$, 1 and Na$_2$MoO$_4$ \cdot 2$\text{H}_2$O, 1.5. The mineral nutrients and trace metals were prepared anaerobically and the estimated pH values were 7.95 and 6.93, respectively. The media were stocked in two 5 L Duran vials. In order to maintain an anaerobic environment, the headspaces were flushed with H$_2$/CO$_2$ (80:20, v/v) for 15 min at 0.1 MPa.

Chemostat cultivation: Using different dilution rates (D), i.e. D$_1$ = 0.071/d, D$_2$ = 0.083/d, D$_3$ = 0.1/d and D$_4$ = 0.125/d of the nutrients and fixed amounts of the trace metals (5 mL), the acclimated sludge was grown in 4 chemostats comprising semi-continuously stirred tank reactors of 1 L, each with a 500 mL working volume incubated at 37 ± 2°C. The chemostat reactors were connected to four airtight pumps for the recirculation of H$_2$/CO$_2$ (80:20, v/v). Each pump was
connected to a timer working at 1 min intervals; the flow rate of H₂/CO₂ (80:20, v/v) gas was maintained at 0.83 mL/min at 0.08 MPa to maximize the mass transfer between the gas and the liquid (Coates et al., 1996). The liquid growth culture was taken from the reactors and replaced anaerobically with inorganic nutrients and trace metals at the dilution rates stated above. A new aluminum GL Sciences gas sampling bag (CCK) consisting of two mini valves containing pure H₂/CO₂ gas was connected to the recirculation gas system at 24 h intervals to obtain a daily estimate of the CH₄ gas produced during the experiment until a the steady state fermentation was achieved.

2.4. Analytical methods

The composition of the gas produced was determined using a GC-14B (Shimadzu) gas chromatograph equipped with a thermal conductivity detector connected to a C-R8A data analyzer. A high performance column packed with 50/80 mesh Porapak Q was used. The temperatures of the injection, column and detector were set to 100, 50, 100°C, respectively. Argon was used as the carrier gas at a pressure of 0.5 MPa. The total solids (TS), volatile suspended solids (VSS) and volatile solids (VS) were determined with 5 duplicate analyses to ensure accuracy of the results obtained, according to the Standard Methods for
Examination of Water and Wastewater (APHA, 2005). The data were subsequently averaged; the deviations obtained were found to be less than 4%. The pH was monitored in situ. Cell number was estimated by a direct count using fluorescence microscopy (OLYMPUS, BX 50).

3. Results and Discussion

3.1. Steady state characteristics of chemostat H₂/CO₂-dependant methanogens

Table 2 shows the measurements of the decrease in the gas concentration from the replaced aluminum gas sampling CCK bag. In the steady state, the percentage consumption rates of H₂ and CO₂ estimated individually, are approximately equal, and the equilibrium ratio did not change with variations in the dilution rates. The results suggest that the H₂/CO₂ complex gas mixture can be considered as a single substrate during the determination of the kinetics parameters of these bacteria. The pH was not found to be a significant factor in the inhibition of bacterial activity within the continuously flowing reactor (Keshtkar et al., 2003) for any dilutions; this is due to the buffering effect of the media and the dissolved H₂/CO₂ in the liquid. However, the inhibitory effect of pH on the physiological activities of hydrogenotrophic methanogens varies among different species.
Costello et al. (1991) presumed that the Monod kinetics can be regarded as a mechanism for correction of the pH inhibition during the determination of the kinetic parameters. As presented in Fig.1, cell production under these conditions illustrates that the biomass concentration decreases with an increase of dilution, data similar to the results obtained by Haydock et al. (2004). The daily cells generated measurements were $5.67 \times 10^{11}$, $5.25 \times 10^{11}$, $4.2 \times 10^{11}$ and $2.1 \times 10^{11}$ cells/L-culture for 0.073/d, 0.083/d, 0.1/d and 0.125/d, respectively. No bacteria carrier was used in the different reactors; thus, the dilution effect explains the data. The specific methanogenic activity (SMA) at different dilutions was determined according to the Ahring and Sorensen (1993) and the results are presented in Fig. 2. The specific methane production rate was varied from 0.6 to 0.7 mmol/g cell hr, values lower than the 7.5 to 11.3 mmol/g cell hr determined by Wise et al. (1978) under the same conditions for a cell recycling system. In the steady state, the highest hydrogenotrophic methanogen activity was observed at a dilution of 0.1/d, 0.24 L CH$_4$/g VSS d, due to the low quantities of trace metals available at low dilution rates. The methanogenic activity plot suggests a decoupling mechanism of anabolism and catabolism with regard to the metabolic activity of
hydrogenotrophic methanogens (Schönheit et al., 1980; Fardeau et al., 1987).

3.2. Kinetic evaluation in chemostat reactor using H₂/CO₂ as substrate

In chemostat cultivation, the Monod equation is expressed as follows:

\[
\frac{1}{D} = \frac{K_s}{\mu_{\text{max}}} \frac{1}{S} + \frac{1}{\mu_{\text{max}}} \tag{2}
\]

where \( D \) is the dilution rate (1/d).

Under steady state conditions, the bacterial growth yield \( (Y_{X/S}) \) is expressed as follows:

\[
Y_{X/S} = \frac{X}{S_0 - S} \tag{3}
\]

where \( S_0 \) and \( S \) represent the concentration of substrate (g/L) at the start of the experiment and at time \( t \), respectively. \( X \) represents the biomass concentration (g/L).

Considering the complex gas mixture of H₂/CO₂ as a single substrate, \( K_s \) and \( \mu_{\text{max}} \) were determined from Eq. (2) (Lee, 1992). The experimental results from the chemostat cultivation showed a maximum growth yield of 11.66 g cells
for each mmol of H₂/CO₂ substrate consumption. This growth rate was found to be higher than the ranges of 0.0053~0.0095 g/mmol and 0.00279~0.0079 g/mmol that were obtained using a pure mixture of *Methanosarcina* sp. strain 227 and *Methanosarcina mazei* under H₂/CO₂ in media containing minerals (Ferguson and Mah, 1983). The operational design of our experiment reveals a good productive fermentation system. The saturation constant $K_S$ was 0.82 g/L, greater than the 0.116 g/L that is necessary for methanogenic bacteria when they compete with sulphate-reducing bacteria for acetate (Bhattacharya et al., 1996) or other substrates (Gilardo-Gomez et al., 1992). With inorganic materials as substrate, it is suggested that a high concentration of H₂/CO₂ is necessary to achieve the cells production. However, the maximum specific growth obtained with H₂/CO₂ as a unique substrate was 0.15/d, and it is 10 times lower than the concentration 1.5/d that was reported for H₂ and CO₂ when acclimated mesophilic methanogen culture was grown using separate organic substrates for H₂ and CO₂ (Zhang and Maekawa, 1994). The flow rate of the gas mixture applied in the present study was 8.3 mL/min, a value substantially lower than that applied by Zhang & Maekawa (1994). The results presented here correspond well with those of
previous literature regarding the maximum specific growth rate as a function of
gas flow rate (Schill et al., 1996).

3.3. Simulation

To simulate the behavior of the substrate ($S$), the cell production rate
($DX$) and the cell concentration ($X$) in the chemostat reactor under steady state
conditions, the following relations are used:

$$ S = \frac{K_S D}{\mu_{\text{max}} - D} $$  \hspace{1cm} (5)

$$ X = Y_{X/S} \left( S_0 - \frac{K_S D}{\mu_{\text{max}} - D} \right) $$  \hspace{1cm} (6)

$$ DX = Y_{X/S} D \left( S_0 - \frac{K_S D}{\mu_{\text{max}} - D} \right) $$  \hspace{1cm} (7)

The washout occurs when the cell concentration is equal to zero

$$ D_{\text{crit}} = \mu_{\text{max}} \frac{S_0}{K_S + S_0} $$  \hspace{1cm} (10)

The slow growth of the CO$_2$-reducing methanogens normally involve a
retention time greater than 10 d for efficient and stable operation (Zinder, 1993).

Fig. 3 summarizes the predictive plots for the hydrogenotrophic methanogen
growth and substrate supply at different dilution rates. The graphs indicate the maximum bacterial rate of growth at low dilution. This amount decreases as the dilution increases until it reaches $D_m$, the maximum dilution where the amount of bacteria in the reactor due to the dilution rate is in equilibrium with the limited supply of nutrients and trace metals. Subsequently, the cell washout begins to reach $D_{crit}$ at the high dilution rate of 0.14/d; the predicted $D_m$ was estimated as 0.11/d. However, the cell production rate ($DX$) increases with increasing dilution rate. The experimental data were in agreement with the predictive plots. The proposed operation system shows that the rates of dilution must be around 0.11/d to attempt a short retention time and a high substrate conversion rate at relatively low cell concentration in order to obviate the problems due to long retention time and toxicity effects of the trace elements. In the present study, the methanogenic bacteria attain an efficient activity level after a short retention time. This prediction was verified by the SMA previously determined (Fig. 2) where the highest methanogenic bacterial activity was 0.24 L CH$_4$/g VSS.d, detected at 0.1/d; this value was found to be close to the predicted value of $D_m$, which was 0.11/d. The predicted critical dilution ($D_{crit}$) value was 0.14/d. The CH$_4$ production effectively dropped when the dilution increased beyond $D_{crit}$. Table 3
presents a suitable range of parameters for chemostat cultivation with a mixture of H₂/CO₂ (80:20, v/v) as substrate which can serve to design a reactor plant.

4. Conclusion

Four anaerobic continuously stirred tank reactors containing cultures of acclimated hydrogenotrophic methanogen, obtained from a domestic anaerobic wastewater treatment plant, were run at different dilution rates in order to obtain engineering data necessary to simulate steady state chemostat cultivation with a supply of inorganic substrate. Under the conditions of steady state cultivation, the Monod model was applied to determine the kinetic parameters, $\mu_{max}$ and $K_S$. The values found were 0.15/d and 0.82 g/L, respectively. From these results, a simulation was performed to predict the dilution rates at which bacteria washout began and at which maximum bacterial activity could be achieved for a concentration of 11.14 g/L of H₂/CO₂. The critical dilution rate for the chemostat was 0.14/d, and the maximum bacterial activity occurred at 0.11/d. The predictions agreed with the data obtained; in addition, the maximum methane gas production rate of 1.21 L/d was achieved at a dilution of 0.1/d. Thus, the engineering results can be summarized and applied to the large scale use of
H$_2$/CO$_2$-dependant methanogens for biogas production using only inorganic substrates. The results demonstrated that, at steady state, the concentration of cells was related more closely to the dilution rate than the H$_2$/CO$_2$ concentration.

Acknowledgements

This research was partially supported by the Ministry of Education, Science, Sports and Culture, Grant-in-Aid for Scientific Research, 14560216, 2003.

References


Batstone, D.J., 2006. Mathematical modelling of anaerobic reactors treating


methane production and methanogenic populations in acidic West-Siberian peat bog. Environ. Microbiol. 6, 1159-1173.


unstructured mathematical model and experimental verification with


Schönheit, P., Moll, J., Thauer, R.K., 1980. Growth parameters (K_S, µ_max, Y_S) of


