

1 Bioactivity of the Crude Polysaccharides from Fermented
2 Soybean Curd Residue by *Flammulina velutipes*

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24 Abstract

25 The solid-state fermentation, reusing soybean curd residue (SCR) as a solid
26 substrate, was conducted for producing polysaccharides by *Flammulina velutipes* (*F.*
27 *velutipes*). The optimal fermentation conditions were 74.5% of moisture content, 9.69
28 of inoculum size and 30.27 of C/N ratio by response surface methodology. 59.15 mg/g
29 of polysaccharides were obtained. *F. velutipes* polysaccharides were subsequently
30 extracted from fermented SCR by ultrasonic assisted extraction. The optimal extract
31 conditions were 30 min, 80 °C, 150 watt and 20 of water to solid ratio and 106.74
32 mg/g of polysaccharides were obtained. Furthermore, the antioxidant and the
33 immunomodulatory activities of polysaccharides were assessed. The results showed
34 that polysaccharides exhibited a strong DPPH radical scavenging activity, SOD-like
35 activity, stimulatory the proliferation of the macrophage, the production of nitric
36 oxide, phagocytosis and the protection on Doxorubicin damage. These could lay the
37 foundation for changing SCR into a nutritious functional food or a food additive.

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39 **Keywords:** Soybean curd residue, *Flammulina velutipes*, Polysaccharides,
40 Macrophages, Antioxidant activities, Immunomodulatory activities

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46 1. Introduction

47 In recent years, there has been an unprecedented increase in interest in the more
48 efficient utilization of the agro-industrial residues because their application provide an
49 alternative way to reduce the production costs and solve many environmental hazards
50 (Qijun, *et al.*, 2008). Soybean curd residue (SCR), a by-product of tofu, soymilk or
51 soy protein manufacturing, is discharged as an agro-industrial waste. 0.7 million tons
52 of SCR is disposed in Japan annually, and the most of SCR was incineration, which
53 has caused severe environmental pollution. In fact, SCR contains the protein up to
54 25.4–28.4% (dry basis) with the high nutritive quality and a superior protein
55 efficiency ratio, suggesting that SCR is a potential source of low-cost vegetable
56 protein for human consumption (Kasai, *et al.*, 2004; O’Toole, 1999). In addition to,
57 this material was rich in the fat, the starch and the sugar, which could allow them to
58 be potentially utilized as a high quality media for the microbial fermentation. Many
59 researchers have investigated the possibility of bioconversion of the residues by
60 submerged and solid-state cultivation (SSC) (Adams, Eiteman, & Hanel, 2002; Holker,
61 & Lenz, 2005; Pandey, Soccol, Nigam, & Soccol, 2000; Yokoi, Maki, Hirose, &
62 Hayashi, 2002).

63 *Flammulina velutipes* (*F. velutipes*) is a cultivated mushroom. Few studies,
64 however, have been conducted on this species. An alkaline protease and the antitumor
65 activities have been reported from this mushroom (Cui, *et al.*, 2006; Wang, Hu, Liang,
66 & Yeh, 2005). Both methanolic and ethyl acetate extracts of this mushroom exhibited
67 anti-hyperlipidemic and antioxidant activities (Hu, *et al.*, 2006). As a result of its

68 perceived health benefits, *F. velutipes* has become one of the valuable mushrooms in
69 China.

70 The low immune function of an organism may not only result in the generation and
71 development of a tumor, but may also be one of the most important factors that
72 prevent the tumor patient's recovery. Immunomodulation through natural or synthetic
73 substances may be considered an alternative for the prevention and cure of diseases.

74 Macrophages play a significant role in the host defense mechanism. When activated,
75 they activate phagocytic activity, produce and release reactive oxygen species (ROS)
76 and the nitric oxide (NO) in response to the stimulation with various agents and can
77 inhibit the growth of a wide variety of tumor cells and micro-organisms (Schepetkin,
78 *et al.*, 2008). Moreover, the immunomodulatory activity not only involves effects on
79 macrophage activation but also on cell proliferation and differentiation (Schepetkin,
80 & Quinn, 2006). Papers report that polysaccharide from the mushroom can enhance
81 and activate the macrophage immune responses, leading to immunomodulation,
82 anti-tumor activity, wound-healing and other therapeutic effects (Berner, Sura, Alves,
83 & Hunter, 2005; Sakurai, Kaise, Yadomae, & Matsubara, 1997).

84 Up to now, *F. velutipes* polysaccharides are mainly extracted from the fruiting body
85 growing on the solid culture medium. However, the time for the growth of fruiting
86 body is too long and its product quality is difficult to control. Therefore, it deserves
87 investigation to produce polysaccharides from the mycelia of *F. velutipes* by SSC. As
88 SSC can be more commonly applied than liquid-state cultivation (Lekha, & Lonsane,
89 1994). SSC has also been frequently utilized in the preliminary tests for cultivating

90 the microorganisms under the experimental conditions because it requires less time
91 and less labor intensive than liquid-state cultivation.

92 To achieve higher polysaccharides yield in a SSC, it is a prerequisite to design an
93 optimal production conditions. The single-factor at a time, the most widely used
94 optimization method, does not account for the combined effects of all the influential
95 factors since other factors are maintained arbitrarily at a constant level. In addition, it
96 is time consuming and requires a large number of experiments to determine the
97 optimum levels of the production conditions (Qijun, *et al.*, 2008). However, such
98 drawbacks of the single-factor optimization method can be overcome by statistical
99 optimization techniques (Chen, *et al.*, 2008). Response surface techniques of central
100 composite design (CCD) is an important statistical optimization method which many
101 factors can be optimized simultaneously and much quantitative information can be
102 extracted by only a few experimental trials (Li, *et al.*, 2011). This method has been
103 successfully applied to the improvement of the culture media or the production of
104 primary and secondary metabolites in the cultivation process of many edible and
105 medicinal mushrooms (Chang, Tsai, & Houn, 2006; Chen, *et al.*, 2008). However,
106 there is still a lack of knowledge concerning SSC conditions for the production of
107 polysaccharides from *F. velutipes* by statistical optimization techniques.

108 Therefore, the objective of this study is to estimate the optimum technology of the
109 fermentation of *F. velutipes* polysaccharides by response surface technology. *F.*
110 *velutipes* polysaccharides of fermented SCR were subsequently extracted by the
111 ultrasonic assisted technology to investigate the antioxidant activities and the

112 immunomodulatory activities on macrophage RAW 264.7 cells.

113 2. Materials and methods

114 2.1 Chemicals and reagents

115 Minimum Essential Medium Eagle (MEM) medium, fetal bovine serum (FBS),
116 were purchased from Sigma Aldrich, Inc. (Saint Louis, MO, USA). Acetic anhydride,
117 pyridine hydroxylamine hydrochloride, trifluoroacetic acid lipopolysaccharide (LPS)
118 from *E. coli* 055 was purchased from Wako Pure Chemical Industries, Ltd. (Osaka,
119 Japan), Cell Counting Kit-8 (CCK-8) was purchased from Dojindo Molecular
120 Technologies, Inc. (Kumamoto, Japan), Doxorubicin (DOX) was purchased from
121 TopoGEN, Inc. (Florida, USA).

122 2.2 Cell lines

123 The murine macrophage cell line, RAW 264.7 was obtained from the Riken Cell
124 Bank (Tsukuba, Japan) and maintained in MEM medium containing 10% fetal bovine
125 serum, 100 U/mL penicillin and 100 µg/mL of streptomycin at 37 °C in a humidified
126 5% CO₂ atmosphere (ESPEC CO₂ Incubator). The cells were cultured for 2-3 days to
127 reach the logarithmic phase and then used for experiments.

128 2.3 Microorganism and culture conditions

129 The A16 strain of *F. velutipes* was purchased from agriculture and forestry strains
130 Kaishas, Japan. D-glucose, sucrose, peptone, KH₂PO₄, MgSO₄, potato extract, agar
131 were obtained from Wako Pure Chemical, Osaka, Japan.

132 The strain was maintained on potato dextrose agar (PDA) at 4 °C. To maintain the
133 strain activity, a mycelium square of size 5 mm × 5 mm was transferred to a fresh

134 PDA agar every 3 months. The activation medium (Yang, & Liao, 1998) consisted of
135 the following components: 2% glucose, 2% peptone, 0.4% potato extract, 0.3%
136 KH_2PO_4 , 0.15% MgSO_4 , 2% agar. The initial pH was not adjusted (5.0-5.5). The
137 mycelial agar petri dish was incubated at 25 °C for 7 days. The 15-mL liquid culture
138 was performed in a 50-mL flask containing one unit of mycelial agar, which was a 5
139 mm × 5 mm square that was obtained using a self-designed cutter on a rotary shaker
140 at 100 rpm and 25 °C for 6 days. The flask of the liquid culture medium was
141 composed of the following components: 2% sucrose, 2% yeast extract, 0.4% potato
142 extract, 0.1% NaCl, 0.3% KH_2PO_4 , 0.15% MgSO_4 . The initial pH was from 5.0 to 5.5.
143 The seed for the solid culture was from the liquid culture. The solid-state culture
144 experiment was performed in a 200-mL flask with the wet SCR in the different culture
145 conditions and incubated at 25 °C. All of the media were autoclaved at 121°C for 30
146 min.

147 2.4 The polysaccharides determination

148 2.4.1 Crude polysaccharides extraction

149 The treatment of the crude *F. velutipes* polysaccharides was according to a
150 literature procedure with a few modifications (Di, *et al.*, 2011). The fermented SCR
151 was dried in a convection oven at 50 °C and ground to a powder. The crushed
152 powder was removed the impurities for 24h with 80% ethanol at room temperature.
153 The extract was discarded and the residue was further extracted with the optimal
154 conditions of ultrasonic assisted extraction. Then, the extract was filtered and
155 centrifuged at 7500 rpm for 30 min at room temperature. The supernatant was

156 concentrated in a rotary evaporator under reduced pressure at 50 °C and removed
157 free protein layer by the use of method of Sevage. At last, the above extract was
158 subjected to the precipitation with eight-fold volumes of ethanol. The curd
159 polysaccharides were collected by centrifugation, washed with ethanol twice, and
160 then freeze-dried and total polysaccharide was the subtraction of reducing sugar
161 from the total carbohydrate.

162 2.4.2 Determination of total carbohydrate content

163 The carbohydrate contents were determined by the phenol-sulfuric acid method
164 with certain modifications. (Mauro, 2005). The color reaction was initiated by mixing
165 1 mL of polysaccharides solution with 0.5 mL of a 5% phenol solution and 2.5 mL of
166 concentrated sulfuric acid, and the reaction mixture was incubation in a boiling water
167 bath for 15 min. After cooling to the room temperature, the optical density (O.D.) of
168 the mixture was determined at 490 nm and the total carbohydrate content were
169 calculated with D-glucose as a standard. The results were expressed as milligram of
170 D-glucose equivalent per gram of fermented SCR.

171 2.4.3 Determination of reducing sugar

172 Reducing sugar content was analyzed by dinitrosalicylic (DNS) colorimetric
173 method (Miller, 1959), using d-glucose as a standard. For each of the 1 mL of the
174 sample, 2 mL of DNS reagent and 12 mL deionized water were added. The mixture
175 was then heated in boiling water for 5 min until the red brown color was developed.
176 Then, the mixture was cooled to room temperature in a water bath. The absorbance
177 was then measured at 540 nm. The concentration of total reducing sugars was

178 calculated based on a standard curve obtained with D-glucose.

179 2.4.4 Monosaccharide analysis

180 The crude polysaccharides (10 mg), dissolved in 2 M trifluoroacetic acid (TFA, 2
181 mL), was hydrolyzed at 120 °C for 3 h in a sealed glass tube. The hydrolyzate was
182 repeatedly co-concentrated with methanol to remove the excess acid at 50 °C, and
183 then the hydrolyzed products were prepared for acetylation. The acetylation was
184 carried out with 10 mg hydroxylamine hydrochloride and 0.5 mL pyridine by heating
185 in a water bath for 30 min at 90 °C. After incubation, the tubes were removed from
186 the heat block, allowed to cool to room temperature, and then 0.5 mL of acetic
187 anhydride was added and mixed thoroughly by vortexing. The tubes were sealed and
188 incubated in a water bath shaker set at 90 °C for 30 min again. After cooling,
189 approximately 0.1 mL of clear supernatant was added to the autosampler vials with
190 inserts for injection into the gas chromatograph on a GCMS-QP2010Plus
191 (SHIMADZU, JAP) instrument equipped with a hydrogen flame ionization detector,
192 using a DB-1 column (30 m × 0.25 mm × 0.25 μm). The following chromatographic
193 conditions were used: high-purity helium was used as the carrier gas at a flow rate of
194 1 mL/min. The temperature of the injector and detector was 250 °C. An initial
195 column temperature held at 60 °C for 2 min followed by 15 °C/min to 180 °C and
196 then 4 °C/min to 250 °C for 3 min. Injections were made in the splitless mode. The
197 temperature of mass spectrometer ion source was 250 °C. 1 μL sample was injected
198 into the column with the split ratio of 10:1.

199 2.5 Antioxidant properties

200 2.5.1 DPPH radical scavenging activity

201 The free radical scavenging activities of the extracts were measured by using
202 1,1-diphenyl-2-picryl-hydrazyl (DPPH •) (Shuang li, *et al.*, 2011). Briefly, 0.2 mL of
203 polysaccharides extract at various concentrations was added to 3.3 mL of DPPH
204 solution (25 µg/mL) for 30 min at room temperature in the dark. Methanol was used
205 instead of polysaccharides extract as the control. Then the absorbance was measured
206 at 517 nm. The capability to scavenge the DPPH radical was calculated using the
207 following equation: DPPH scavenging effect (%) = $[(A_0 - A_1/A_0) \times 100]$, where A_0
208 was the absorbance of the control reaction and A_1 was the absorbance in the presence
209 of the sample. The extract concentration providing 50% inhibition (IC_{50}) was
210 calculated from the graph of DPPH scavenging effect against the extract concentration.
211 Ascorbic acid was used as the positive control.

212 2.5.2 Determination of SOD-like activity

213 The levels of SOD-like activity in the extracts were measured using the SOD Assay
214 Kit-WST according to the technical manual provided by Dojindo Molecular
215 Technologies, Inc. Briefly, in a 96-well plate, 20 µL of sample solution was added to
216 each sample and blank 2 well, and 20 µL of double distilled water was added to each
217 blank 1 and blank 3 well. Then 200 µL of WST working solution was added to each
218 well. After mixing, 20 µL of dilution buffer was added to each blank 2 and blank 3
219 well, and 20 µL of enzyme working solution (15 µL of enzyme mixed with 2.5 µL
220 dilution buffer) was added to each sample and blank 1 well. The plate was incubated
221 at 37 °C for 20 min and the O.D. was determined at 450 nm using a microplate

222 reader (BIO-RAD Model 550, USA). The SOD-like activity was calculated by the
223 following equation:

224 SOD activity (inhibition rate %) =
225
$$\{[(A_{\text{blank1}}-A_{\text{blank3}})-(A_{\text{sample}}-A_{\text{blank2}})] / (A_{\text{blank1}}-A_{\text{blank3}})\} \times 100 \quad (1)$$

226 Where $A_{\text{blank 1}}$, $A_{\text{blank 2}}$, $A_{\text{blank 3}}$ and A_{sample} were the absorbance of blank 1, blank
227 2, blank 3 and the sample respectively.

228 2.6 Cell evaluation

229 2.6.1 Activation assay

230 The effect of *F. velutipes* polysaccharides on the proliferation of RAW 264.7 cells
231 was estimated using the Cell Counting Kit-8 (CCK-8). RAW 264.7 cells were
232 cultured in a 96-well plate at a density of 5×10^4 cells/mL at 37 °C in a 5% CO₂
233 atmosphere for 24 h. Next the cells were incubated with various concentrations of
234 polysaccharides (1.25, 2.5, 5, 10, 20 and 40 µg/mL) at 37 °C for 24 h. After
235 incubation, 10 µL of CCK-8 solution was added and incubated at 37 °C for 4 h. The
236 cell viability was assessed by the O.D. at a wavelength of 450 nm with a microplate
237 reader (BIO-RAD Model 550). The data were expressed as the percentage of the
238 control.

239 2.6.2 Measurement of the production of the nitric oxide

240 The nitrite accumulation was measured using Griess reagent and used as an
241 indicator of nitric oxide (NO) production in the medium (Di, *et al.*, 2011;
242 Gamal-Eldeen, *et al.*, 2007). The macrophage cells (1×10^5 cells/mL) were dispensed
243 into a 96-well plate for 24 h. Next the cells were stimulated with LPS (1 µg/mL) and

244 various concentrations of *F. velutipes* polysaccharides (2.5, 5, 10, 20 and 40 µg/mL)
245 for 24 h. After the incubation, 50 µL of the culture supernatants were mixed with an
246 equal volume of Griess reagent in a 96-well plate and incubated at 25 °C for 10 min.
247 The absorbance at 570 nm was measured on a microplate reader. The nitrite
248 concentrations in the culture supernatants were measured to assess the NO production
249 in the RAW 264.7 cells. NaNO₂ was used as a standard to calculate the nitrite
250 concentrations.

251 2.6.3 Phagocytosis assay

252 The phagocytic ability of the macrophage was measured by the neutral red uptake
253 (Cheng, *et al.*, 2008). The cells were cultured in a 96-well plate at a density of 5×10^4
254 cells/mL at 37 °C in a 5% CO₂ atmosphere for 24 h. Next the cells were incubated
255 with various concentrations of *F. velutipes* polysaccharides (1.25, 2.5, 5, 10, 20 and 40
256 µg/mL) and LPS (1 µg/mL) at 37 °C for 48 h. 100 µL of 0.075% neutral red solution
257 was added and incubated for 1 h. Then the supernatant was discarded and the cells
258 were washed with PBS twice. Then 100 µL of the cell lysate solution (ethanol and
259 0.01% acetic acid at the ratio of 1:1) was added into a 96-well plate to lyse the cells at
260 the room temperature for 2 h. The optical density at 570 nm was measured by a
261 microplate reader (BIO-RAD Model 550).

262 2.6.4 Protective activity

263 The macrophages RAW 264.7 cells were cultured in a 96-well plate at a density of
264 5×10^4 cells/mL for 24 h at 37 °C in a 5% CO₂ atmosphere. Next the cells were
265 incubated with DOX (5 µM) in the presence or absence of various concentrations of *F.*
266 *velutipes* polysaccharides (2.5, 5, 10 and 20 µg/mL) for 24 h. After the drug exposure,

267 10 μ L of the CCK-8 solution was added and incubated at 37 °C for 4 h. The cell
268 numbers were quantitated by reading the absorbance at 450 nm. The data were
269 expressed as the percentage of the control.

270 2.7 *Experimental design*

271 2.7.1 The optimization using response surface methodology

272 RSM is a collection of mathematical and statistical technique for building the
273 empirical models. It was applied to evaluate the relationship of the
274 environmental factors and to determine the optimum conditions under which the
275 mycelia growth is the maximum, within the experimental range of the independent
276 variables (Hwanyoung, Minkyung, & Seokhwan, 2003). In this study, RSM was used
277 to assess the relationship of the radial extension rate to the fermentation conditions
278 (the inoculum size, the moisture content and the C/N ratios).

279 The experiment (Table 1) was based on the central composite in the cube design
280 and consisted of a 3×2 the central composite design (CCD) (the inoculum size, the
281 moisture content and the C/N ratio, each at two levels). The ranges of the independent
282 variables were 7.5% to 12.5% of the inoculum size, 60% to 80% of the moisture
283 content and 20 to 40 of the C/N ratios. Each treatment with a center point (i.e., 10% of
284 the inoculum size, 70% of the moisture content and 30 of the C/N ratio) was
285 replicated 5 times as previously described. This type of design was used to minimize
286 the number of the trials needed to obtain statistically the valid results.

287 A sequential procedure of collecting data, estimating polynomials, and checking the
288 adequacy of the model was used. The method of least squares was used to estimate

289 the parameters in the approximating polynomials. For the statistical analysis,
290 Stat-Ease Design-Expert 8.0.5 (Stat-Ease Corporation, USA) was used to establish the
291 experimental design and to test the complex polynomials.

292 2.7.2 The orthogonal array design

293 *F. velutipes* polysaccharides were extracted from fermented SCR by ultrasonic
294 assisted extraction and the extract process was optimized through the orthogonal array
295 design table of L₉(3⁴) shown in Table 2 (Xiong, Shouwen, Ming, & Ziniu, 2005).

296 3. Results and discussion

297 3.1 Parameters of the solid-state cultivation of *F. velutipes* polysaccharides using 298 response surface methodology

299 Based on the single-factor experiment, three variables (the inoculum size, the
300 moisture content and the C/N ratios) were used to determine the optimum levels of
301 these parameters and their interactions according to 20 days of fermentation time and
302 5.5 of pH value. There was a considerable variation in the yield of polysaccharides
303 depending upon the fermentation conditions, as shown in Table 3. The replication at
304 the center point conditions resulted in a higher yield of polysaccharides than at the
305 other levels. The predicted response *Y* for the production of polysaccharides was
306 obtained as follows:

$$307 \quad y = -371 + 23.99x_1 + 6.5x_2 + 4.75x_3 - 0.01x_1x_2 \quad (2) \\ \quad \quad \quad + 0.27x_1x_3 + 0.02x_2x_3 - 1.63x_1^2 - 0.05x_2^2 - 0.14x_3^2$$

308 The statistical significance of Eq. (2) was confirmed by an F-test and the analysis of
309 variance (ANOVA) for the response surface quadratic model summarized in Table 4.

310 The ANOVA of the quadratic regression model demonstrated that the model was
311 significant, with an F-test of a very low probability value ($P > F < 0.0001$). The
312 goodness of the model was indicated by the determination coefficient (R^2) and the
313 multiple correlation coefficient (R). The value of R^2 (0.993) for Eq. (2) suggested that
314 99.3% of the sample variation for *F. velutipes* polysaccharides was attributed to the
315 independent variables, and only 0.7% of the total variation could not be explained by
316 this model (Pujari, & Chandra, 2000). The “Pred R-Squared” of 0.9040 was in
317 reasonable agreement with the “Adj R-Squared” of 0.9839. The insignificant
318 lack-of-fit showed that the polynomial model was satisfactorily accurate for
319 predicting the relevant responses. The adequate precision was used to measure the
320 ratio of signal to noise, which is generally desired to be greater than 4. In the present
321 study, the value of this ratio (32.681) suggested that the polynomial quadratic model
322 was of an adequate signal, which could be used to navigate the design space (Table 4).

323 The P -values were used as a tool to check the significance of the each coefficient,
324 the smaller the value of P , the more significant was the corresponding coefficient
325 (Rao, Kim, & Rhee, 2000). As can be seen from Table 4, three linear coefficients
326 (X_1 – X_3) and two quadratic coefficients were significant. The insignificant coefficients
327 were still considered in the Eq. (2) because it was a hierarchical model (Wang, & Lu,
328 2004). The 3D-surface plot and 2D-projection were able to visually show the response
329 over a region of the interesting factor levels, the relationship between the response
330 and the experimental levels of each variable, and the type of the interactions between
331 the test variables to deduce the optimum conditions (Fig.1 (A–F)).

332 The 3D-surface plot and 2D-projection (Fig.1 (A, B)) depicted the effects of the
333 inoculum size and the moisture content on the yield of *F. velutipes* polysaccharides,
334 whereas the C/N ratio was fixed at its optimal concentration. The 3D-plot showed that
335 the production of *F. velutipes* polysaccharides significantly increased upon increasing
336 the moisture content to approximately 74%, but decreased sharply beyond this
337 duration, reaching a maximum yield at 74.5%. The effect of the inoculum size on the
338 yield of *F. velutipes* polysaccharides was additionally sensitive within the tested range,
339 reaching a maximum yield at approximately 10. The same trends were indicated in
340 Fig. 1(C-F).

341 By solving the inverse matrix (from Eq. (2)), the optimum values of the test
342 variables were determined to be 74.5% of the moisture content, 9.69% of the
343 inoculum size and 30.27 of the C/N ratio. In this situation, the maximum predicted
344 production of *F. velutipes* polysaccharides were 59.40 mg/g. Cultivated with the
345 optimized conditions, *F. velutipes* polysaccharides of fermented SCR (59.15 ± 1.47
346 mg/g) were accumulated and as much as sevenfold compared with unfermented SCR
347 (8.01 ± 0.54 mg/g).

348 *3.2 The optimization of F. velutipes polysaccharides extraction*

349 There were many factors affecting *F. velutipes* polysaccharides by ultrasonic
350 assisted extraction, such as extracted time, extracted temperature, the ultrasonic power
351 and the ratio of liquid to solid. Based on the orthogonal experiment design $L_9(3^4)$, a
352 total of four factors above, each with three different levels (Table 2), were selected in
353 this study. The results and the effects of those factors on *F. velutipes* polysaccharides

354 extraction were additionally showed in Table 2. Based on the magnitude order of R,
355 the effects of the factors on the extraction of *F. velutipes* polysaccharides decreased in
356 the following order: extracted temperature (B), the ratio of liquid to solid (D),
357 extracted time (A), the ultrasonic power (C). Based on the magnitude order of K
358 (Table 2), the optimal combination was A₃B₃C₃D₂, namely 30 min of the extracted
359 time, 80 °C temperature, 110 watt of the power and 20:1 of the ratio of liquid to solid.
360 The results of the orthogonal experiment additionally showed that all of the single
361 factor effects on the yield of *F. velutipes* polysaccharides were significant (P < 0.01)
362 (Table 5). The mean yield of *F. velutipes* polysaccharides under the optimum
363 extracted conditions was 106.74 ± 1.73 mg/g. *F. velutipes* polysaccharides yield
364 increased approximately 70% against the process parameters before the optimization.

365 3.3 Monosaccharide composition of *F. velutipes* polysaccharides

366 The compositions of the crude *F. velutipes* polysaccharides have been assessed,
367 which contained 88.74% carbohydrates and 0.92% protein. Furthermore, there was
368 0.32% reducing sugar in the extracts, therefore, the percentage of *F. velutipes*
369 polysaccharides was 88.42%.

370 Usually, GC analysis could give the accurate content of sugars in the
371 polysaccharides. The experimental results from GC showed that *F. velutipes*
372 polysaccharides was a typical heteropolysaccharide charide, and the retention times
373 were 11.21, 11.39, 11.52, 13.73, 13.83, 14.08 and 15.04 min for rhamnose, arabinose,
374 xylose, mannose, glucose, galactose and myo-inositol, respectively. After
375 identification and quantitation, GC chromatogram showed six monosaccharides

376 including rhamnose, arabinose, xylose, mannose, glucose and galactose to be present
377 in *F. velutipes* polysaccharides at a molar ratio of 0.42: 0.37: 1.3: 1.79: 3.38: 0.46,
378 respectively.

379 *3.4 Antioxidant activities of F. velutipes polysaccharides*

380 *3.4.1 Scavenging activity of DPPH radicals*

381 ROS produced the in vivo including superoxide radical, hydrogen peroxide and
382 hypochlorous acid. Hydrogen peroxide and superoxide can interact in the presence of
383 certain transition metal ions to yield a highly-reactive oxidising species, the hydroxyl
384 radical (Halliwell, & Gutteridge, 1985). The antioxidants react with the stable free
385 radical DPPH (deep violet color) and convert it to 1,1-diphenyl-2-picryl hydrazine
386 with decoloration. The scavenging effects of *F. velutipes* polysaccharides increased
387 with the concentrations, around 90% at 2.5 mg/mL of the concentration with 418.31
388 $\mu\text{g/mL}$ of an IC_{50} value, compared with ascorbic acid (293.23 $\mu\text{g/mL}$) (Fig. 2).
389 Previous reports indicated that ascorbic acid and polyphenols exhibited potent DPPH
390 radical scavenging activity, those conjugated with polyphenols such as ferulic acid,
391 have been shown to possess such activity. However, *F. velutipes* polysaccharides
392 extracted with fermented SCR, showed a strong DPPH radical scavenging activity,
393 moreover, its radical free scavenging capacity was superior to those found for several
394 other edible mushroom methanolic extracts (Ferreira, Baptista, Vilas-Boas, & Barros,
395 2007). The results of Rao *et al.* that showed acidic sugars (galacturonic and
396 glucuronic acids), and a hydroxyl group of acidic polysaccharides possessed radical
397 scavenging activity (Rao, & Muralikrishna, 2006). Therefore, the effect observed in

398 this study was likely to be related to the acidic sugar present in *F. velutipes*
399 polysaccharides.

400 3.4.2 SOD-like activity

401 All living bodies have a complex antioxidant defense system that includes various
402 antioxidant enzymes, such as superoxide dismutase and catalase. A rapid and facile
403 method for the assay of SOD-like activity, based on the ability to inhibit the
404 auto-oxidation of pyrogallol, is widely used to predict antioxidant capability. SOD is
405 an antioxidant enzyme that catalyzes the dismutation of superoxide anions into O₂ and
406 H₂O₂ (Mates, Perez-Gomez, & Nunez de Castro, 1999). In the present study, we
407 found that SOD-like activity increased with the concentrations of *F. velutipes*
408 polysaccharides, and treated with *F. velutipes* polysaccharides at the concentration of
409 5 mg/mL, SOD-like activity was 82.48% (Fig. 3).

410 3.5 Evaluation of macrophage RAW 264.7 cells

411 3.5.1 The effect of on the proliferation of the macrophage

412 The stimulatory effect of *F. velutipes* polysaccharides extracted from fermented
413 SCR on the proliferation of the macrophage was tested. The results showed that,
414 exposure to *F. velutipes* polysaccharides activated the proliferation of the macrophage
415 (Fig. 4). In the range of 1.25-40 µg/mL, polysaccharides stimulated the proliferation
416 of RAW 264.7 cells in a dose-dependent manner. At the concentration of 20 µg/mL,
417 the stimulatory effect reached a maximum, was 175.36%. Furthermore, the high
418 concentrations (20-40 µg/mL) were tested on the macrophage. Although the survival
419 rate of the cells decreased dose-dependently at high concentration, this may be related

420 with the immunological paralysis caused by the high dosage (Jinwei, *et al.*, 2011), the
421 survival rate of RAW 264.7 cells at 40 µg/mL was still higher than the control, was
422 106.15%. It was suggested that *F. velutipes* polysaccharides possessed a stimulatory
423 effect on the proliferation of the macrophage RAW 264.7 cells with low cytotoxicity.

424 3.5.2 The effect of *F. velutipes* polysaccharides on the production of the nitric oxide

425 It was reported that LPS showed strong immunomodulating activity (Avni, Ernst,
426 Philosoph, & Zor, 2010). This compound stimulates the macrophages to produce
427 pro-inflammatory cytokines and secondary mediator, such as NO which is a gaseous
428 molecule synthesized from L-arginine by nitric oxide synthase (NOS). It is a highly
429 reactive free radical that can form a number of oxidation products such as NO₂, NO₂⁻,
430 N₂O₃ and S-nitrosothiols. NO participates in the physiology and pathophysiology of
431 many systems (Diouf, Stevanovic, & Boutin, 2009). It is an important mediator of the
432 non-specific host defense against invading microbes and tumors. Thus NO can be
433 used as a quantitative index of the macrophage activation. The results of the
434 stimulatory effect of polysaccharides on the NO production of the macrophage were
435 showed in Figure 5. The data showed that the incubation with polysaccharides
436 stimulated the NO production in RAW 264.7 cells in a dose-dependent manner.
437 Treatment with polysaccharides at a concentration of 40 µg/mL significantly
438 stimulated the NO production (29.11 µM) in comparison with the control (6.32 µM)
439 (p<0.01), and was higher than 20.52 µM of 1 µg/mL LPS (the positive control)
440 produced.

441 3.5.3 Effect of *F. velutipes* polysaccharides on the phagocytosis activity

442 Because the macrophages play an important role in the host defense that
443 phagocytize the pathogens (Zhao, Dong, Chen, & Hu, 2010). Thus phagocytosis is an
444 important indicator of the macrophage effector activity (Yu, *et al.*, 2008) and it
445 represents the final and the most indispensable step of the immunological defense
446 system (Campelo, *et al.*, 2002). The phagocytic activity of the macrophage was
447 monitored by measuring the amount of neutral red internalized in the macrophage.
448 The results were shown in Figure 6. *F. velutipes* polysaccharides significantly and
449 dose-dependently increased the phagocytosis of RAW 264.7 cells in comparison with
450 the control ($p < 0.01$). Moreover, the O.D. value of treatment with *F. velutipes*
451 polysaccharides at 5 $\mu\text{g/mL}$ was higher than that of the positive control, which was
452 treated with LPS at 1 $\mu\text{g/mL}$. The results demonstrated that the administration of *F.*
453 *velutipes* polysaccharides might result in the initiation of the immune reaction against
454 the foreign materials such as pathogen and tumors (WX Chen, Zhang, Shen, & Wang,
455 2010).

456 3.5.4 the protective effect of *F. velutipes* polysaccharides on DOX-induced 457 macrophage viability

458 Doxorubicin (DOX) is a drug used in cancer chemotherapy. It is an anthracycline
459 antibiotic, closely related to the natural product daunomycin, and like all
460 anthracyclines, it works by intercalating DNA. Treatment with DOX resulted in a
461 decrease of the macrophage survival rate, which was 58.45% (Figure 7). However in
462 the presence of *F. velutipes* polysaccharides, the viability of macrophages was
463 significantly higher than that of the incubation with DOX. For example, the

464 incubation with 20 $\mu\text{g/mL}$ of *F. velutipes* polysaccharides, the cell survival rate
465 (93.48%) was significantly higher than the negative control (exposure to 5 μM DOX).
466 When incubated DOX-induced macrophages with the various concentrations of *F.*
467 *velutipes* polysaccharides, the cells survival rate increased in a dose-dependent
468 manner.

469 **4. Conclusions**

470 The production of polysaccharide from *Flammulina velutipes* reusing soybean curd
471 residue was investigated in the solid-state cultures and the optimized culture
472 conditions for polysaccharides were obtained by response surface methodology. In
473 addition, the yield of *F. velutipes* polysaccharides was improved by ultrasonic assisted
474 extraction. Moreover, the extracted *F. velutipes* polysaccharide from fermented SCR
475 showed a strong DPPH radical scavenging activity, SOD-like activity, stimulatory
476 effect on the proliferation of the cells, the NO production, phagocytosis and the
477 protection of the macrophages from DOX damage. These finding indicated that
478 fermented SCR by *F. velutipes* could be a potential and nutritious ecologic feed and a
479 functional food material. Further works are in progress on the isolation, purification,
480 characterization and functional effects of polysaccharide from *F. velutipes* generated
481 by reusing SCR.

482

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596

597

Figure caption

Fig.1 Response surface 3D-surface plot and 2D-projection showing the effects of the inoculum size, the moisture content and the C/N ratio on the yield of *F. velutipes* polysaccharides.

Fig.2 DPPH radical scavenging activity of *F. velutipes* polysaccharides. The data were expressed as means \pm S.D. of triplicate determinations. Ascorbic acid was used as the positive control.

Fig.3 SOD-like activity of *F. velutipes* polysaccharides. The data were expressed as means \pm S.D. of triplicate determinations.

Fig.4 The effect of *F. velutipes* polysaccharides from fermented soybean curd residue on the proliferation of the macrophage RAW 264.7 cells. The cells were incubated with various concentrations of *F. velutipes* polysaccharides (1.25, 2.5, 5, 10, 20 and 40 $\mu\text{g}/\text{mL}$). The data were expressed as means \pm S.D. of three independent experiments. (* $p < 0.05$, ** $p < 0.01$ in comparison with the control).

Fig.5 The effect of *F. velutipes* polysaccharides from fermented soybean curd residue on the nitric oxide production of the macrophage RAW 264.7 cells. The cells were incubated with various concentrations of *F. velutipes* polysaccharides (2.5, 5, 10, 20 and 40 $\mu\text{g}/\text{mL}$) and 1 $\mu\text{g}/\text{mL}$ of LPS for 24 h. LPS was the positive control. The data were expressed as means \pm S.D. (n=3). (** $p < 0.01$ in comparison with the control).

Fig.6 The effect of treatment with *F. velutipes* polysaccharides for 48 h on phagocytosis of the macrophage RAW 264.7 cells. The cells were incubated with various concentrations of *F. velutipes* polysaccharides (1.25, 2.5, 5, 10, 20 and 40 $\mu\text{g}/\text{mL}$) and 1 $\mu\text{g}/\text{mL}$ of LPS for 48 h. The data were expressed as means \pm S.D. (n=3), (** $p < 0.01$ in comparison with the control).

Fig.7 The effect of *F. velutipes* polysaccharides from fermented soybean curd residue on DOX-induced the macrophage RAW 264.7 cells survival rate. The macrophage RAW 264.7 cells were incubated with DOX (5 μM) in the presence or absence of various concentrations of *F. velutipes* polysaccharides (2.5, 5, 10 and 20 $\mu\text{g}/\text{mL}$) for 24 h. The data were expressed as means \pm S.D. (n=3). (* $p < 0.05$, ** $p < 0.01$ in comparison with DOX).

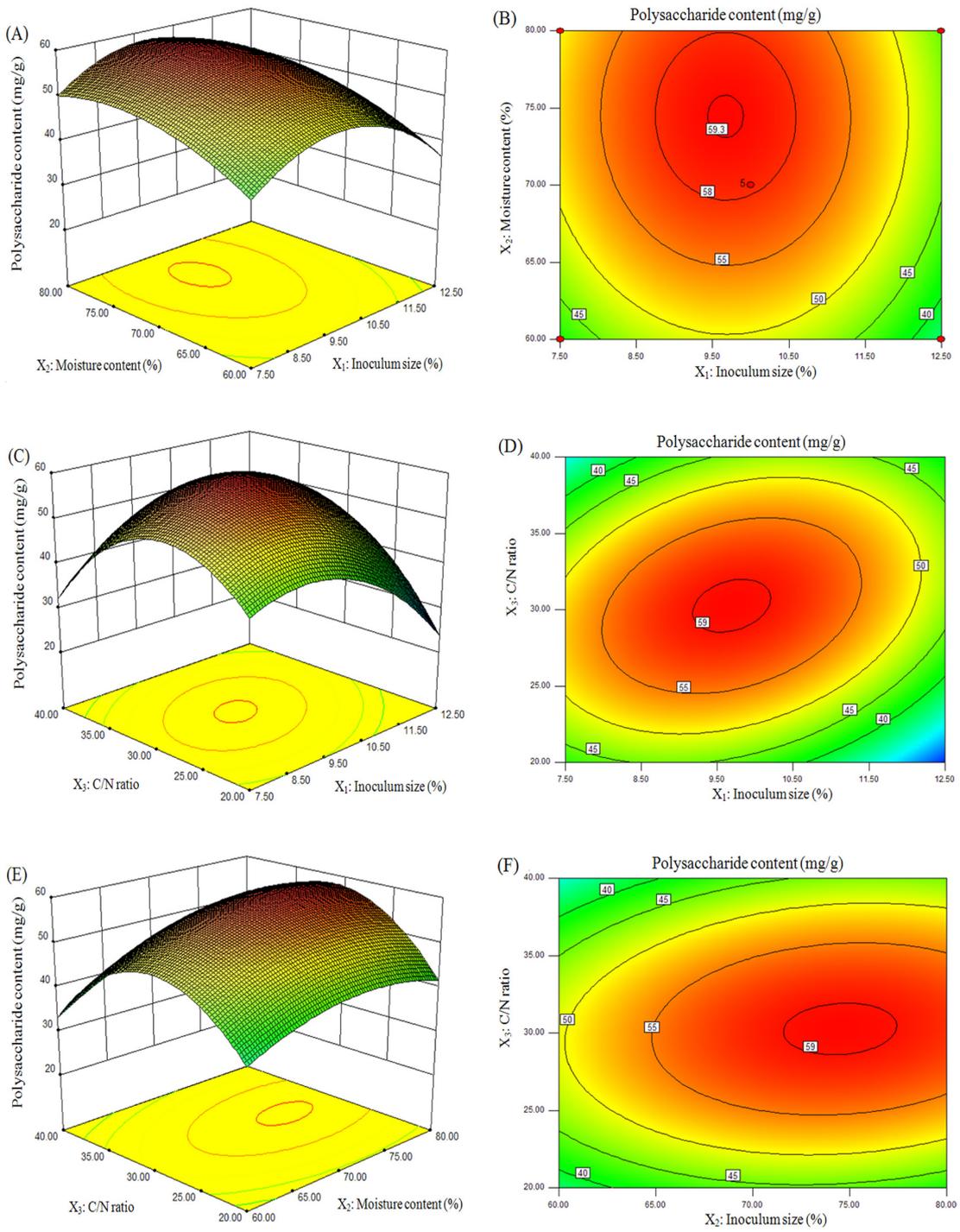


Fig. 1 Shi et al.

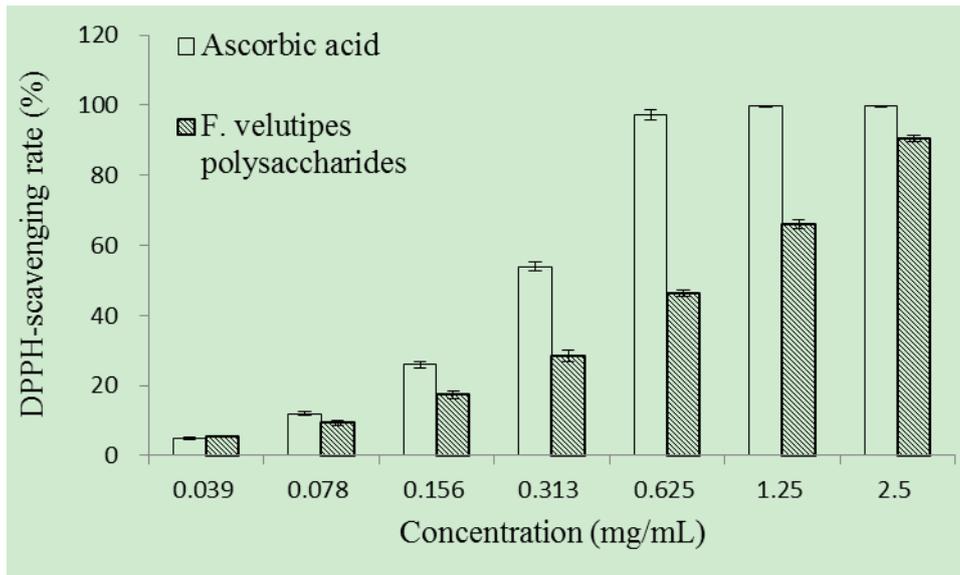


Fig. 2 Shi et al.

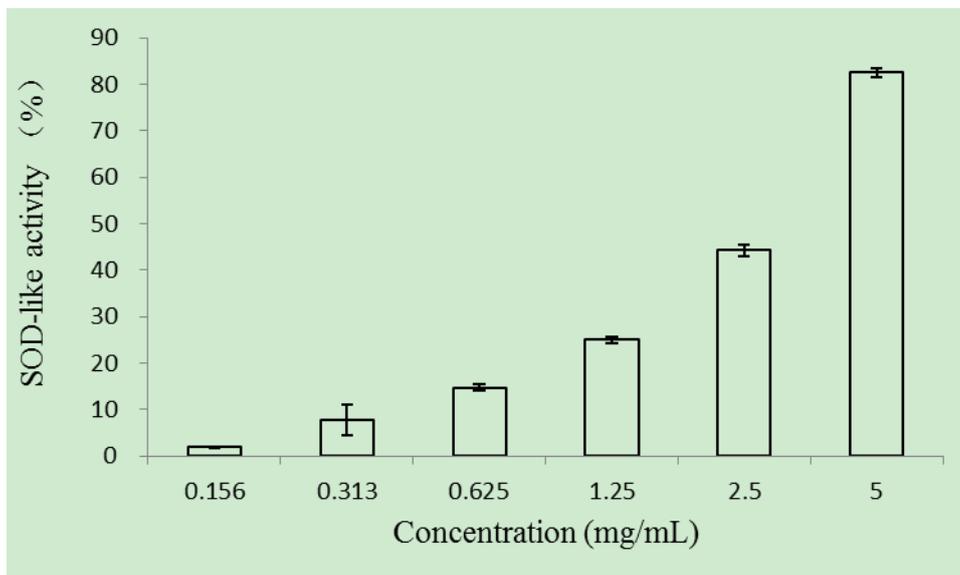


Fig. 3 Shi et al.

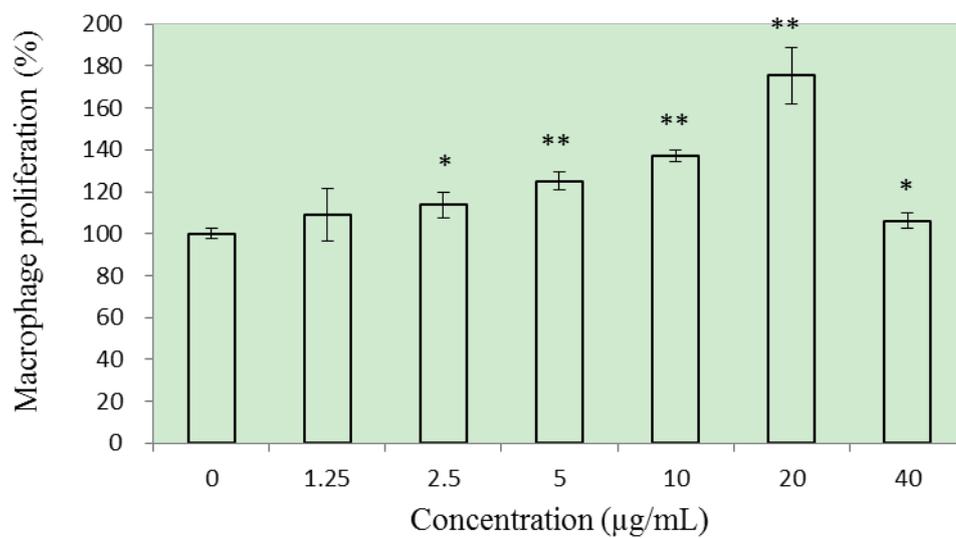


Fig. 4 Shi et al.

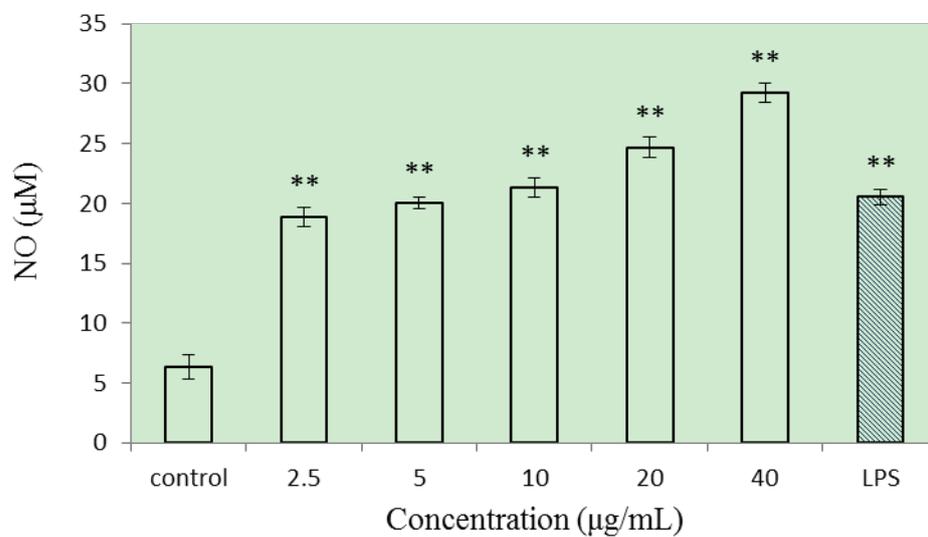


Fig. 5 Shi et al.

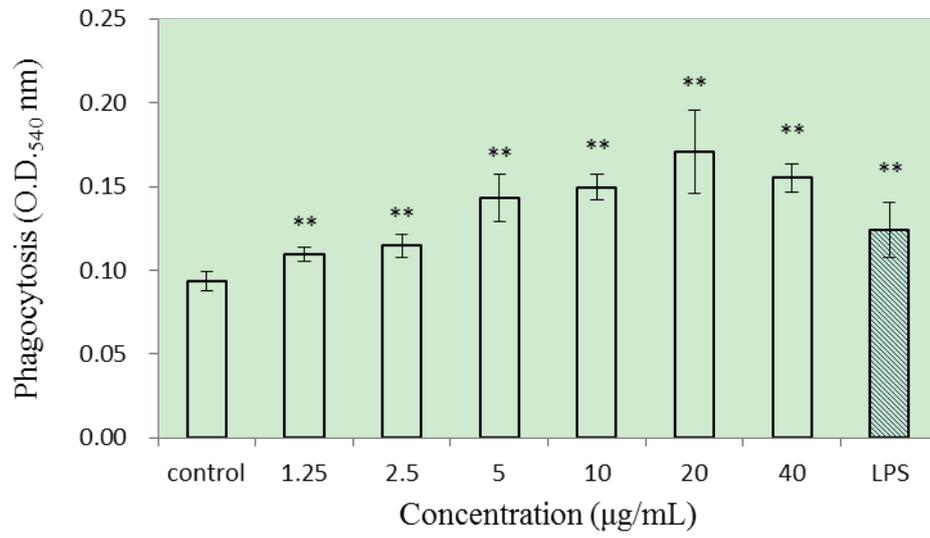


Fig. 6 Shi et al.

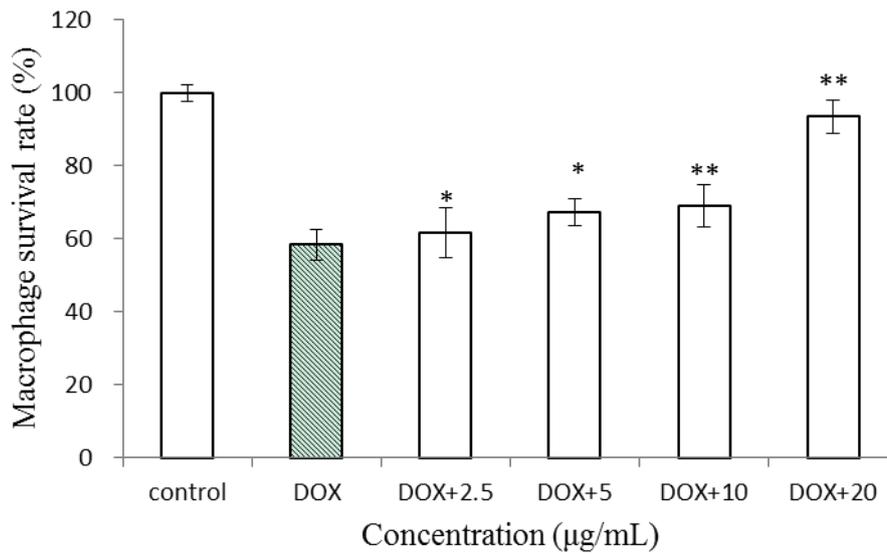


Fig. 7 Shi et al.

Table 1. Independent variable values of the process and their corresponding levels

Independent variable	Unit	Coded variables levels		
		-1	0	1
Inoculum size	%	7.5	10	12.5
Moisture content	%	60	70	80
C/N ratio	—	20	30	40

Table 2. 4-Factor, 3-level orthogonal array used in the original series of the extractions, plus the polysaccharides content of fermented SCR extracts measured by the phenol-sulfuric acid method

Run No.	Factor A Time (min)	Factor B Temp (°C)	Factor C Power (W)	Factor D Liquid: Solid ^a	Polysaccharide (mg/g)
1	10	30	50	10:1	31.89 ± 0.92 ^b
2	10	50	80	20:1	43.18 ± 0.84
3	10	80	110	30:1	61.40 ± 3.15
4	20	30	80	30:1	26.68 ± 1.06
5	20	50	110	10:1	39.04 ± 1.14
6	20	80	50	20:1	49.26 ± 1.72
7	30	30	110	20:1	34.64 ± 0.49
8	30	50	50	30:1	40.29 ± 2.15
9	30	80	80	10:1	82.48 ± 2.18
K ₁ ^c	61.10 ± 3.53	63.90 ± 3.85	60.12 ± 3.12	63.59 ± 4.05	
K ₂	67.28 ± 3.97	58.01 ± 3.32	69.71 ± 4.51	72.24 ± 4.66	
K ₃	73.01 ± 4.81	79.47 ± 5.15	71.55 ± 4.94	60.55 ± 3.55	
R ^d	11.92 ± 1.16	21.46 ± 1.34	11.43 ± 0.93	16.69 ± 1.25	
Optimal level	3	3	3	2	

^a Liquid: Solid was Liquid (mL): Solid (g)

^b Values were mean of three determinations with the standard deviation (±).

^c $K_i^A = \sum$ polysaccharide yield at A_i . Values were mean of three determinations with the standard deviation (±).

^d $R^A = \max\{K_i^A\} - \min\{K_i^A\}$. Values were mean of three determinations with the standard deviation (±).

Table 3. Central composite experimental design matrix, as well as the responses and the predicted values for the polysaccharides content

Run	Independent variable			Polysaccharides content (Y) (mg /g)		
	Inoculum size (%)	Moisture content (%)	C/N ratio	Experimental (Y_0)	Predicted (Y_i)	$Y_0 - Y_i$
1	7.5	60	30	41.42	41.70	-0.28
2	12.5	60	30	37.87	36.71	1.16
3	7.5	80	30	49.10	50.33	-1.23
4	12.5	80	30	45.00	44.80	0.20
5	7.5	70	20	42.30	42.23	0.07
6	12.5	70	20	22.33	23.69	-1.36
7	7.5	70	40	31.90	30.47	1.43
8	10	70	40	44.37	44.67	-0.30
9	10	60	20	36.29	36.12	0.17
10	10	80	20	41.91	40.79	1.12
11	10	60	40	32.90	33.95	-1.05
12	10	80	40	45.90	45.99	-0.09
13	10	70	30	58.40	58.28	0.12
14	10	70	30	57.09	58.28	-1.19
15	10	70	30	58.85	58.28	0.57
16	10	70	30	58.61	58.28	0.33
17	10	70	30	57.61	58.28	-0.67

With 20 days of the fermentation time and 5.5of pH value, the experiment was repeated four times and the response represents average values.

Table 4. Analysis of variance (ANOVA) for the regression equation

Term	degree of freedom	sum of squares	F value	Prob >F	significant
Model	9	1882.79	109.84	< 0.0001	**
X ₁	1	38.91	20.43	0.0027	**
X ₂	1	139.69	73.35	< 0.0001	**
X ₃	1	3.85	2.02	0.1979	
X ₁ X ₂	1	0.074	0.039	0.8489	
X ₁ X ₃	1	95.56	50.18	0.0002	**
X ₂ X ₃	1	13.60	7.14	0.0319	*
X ₁ ²	1	346.61	181.99	< 0.0001	**
X ₂ ²	1	83.43	43.81	0.0003	**
X ₃ ²	1	802.60	421.41	< 0.0001	**
Residual	7	13.33			
Lack of fit	3	9.35	3.14	0.1492	
Pure Error	4	3.98			
Cor Total	16	1896.12			
R ²		0.9930			
Adj R ²		0.9839			
Pred R ²		0.9040			
Adequate Precision		32.681			

With 20 days of the fermentation time and 5.5 of pH value, the experiment was repeated four times and the response represents average values. p* < 0.05, ** p < 0.01

Table 5. Analysis of variance for the orthogonal experiment

Variation source	d.f.	Sum of squares	F value	<i>P</i> value
Time (min)	2	638.01	159.23	< 0.01
Temp (°C)	2	2214.03	552.56	< 0.01
Power (W)	2	678.21	169.26	< 0.01
Liquid (mL): Solid (g)	2	1423.16	355.18	< 0.01
Error	2	32.05		
Sum	16	5007.20		

d.f. : degree of freedom